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ORIGINAL ARTICLE



## Enhancing the performance of supercapacitor electrode from chemical activation of carbon nanofibers derived *Areca catechu* husk via one-stage integrated pyrolysis

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#### Abstract

A carbon nanofiber was produced from the *Areca catechu* ht3 cas a supercapacitor electrode, utilizing a chemical activation of potassium hydroxide (KOH) at different concentrations. One-stage integrated pyrolysis both carbonization and physical activation were employed for directly converting biomass to activated carbon nanofiber. The morph 58 gy structure, specific surface area, pore structure characteris 54 crystallinity, and surface compound were characterized to evaluate the influence on electrochemical performance. The electrochemical performance of the supercapacitor was measured using cyclic voltammetry (CV) through a symmetrical system in 1 M H<sub>2</sub>SO<sub>4</sub>. The results show that the KOH-assisted or absence activation converts activ 5d carbon from aggregate into a unique structure of nanofiber. The optimized carbon nanofiber showed the large specific surface area of 838.64 m<sup>2</sup> g<sup>-1</sup> with the total pore volume of 0.448 cm<sup>3</sup> g<sup>-1</sup>, for enhancing electrochemical performance, including a specific capacitance of 181.96 F g<sup>-1</sup> and maximum energy density of 25.27 Wh kg<sup>-1</sup> for the power density of 91.07 W kg<sup>-1</sup>. This study examines a facile conventional route for producing carbon nanofiber from biomass *Areca catechu* husk in economical and efficient for electrode supercapacitor.

Keywords Activated carbon · Areca catechu husk · Carbon nanofiber · Chemically activation · Supercapacitor

#### 1 Introduction

Energy storage has been extensively studied due to the increasing energy consumption in recent years. This has been contributed by the rapid advancements in technology and the digital era, which have necessitated research on high power and energy density, as well as portable device packaging [1]. Additionally, fossil energy needs to be replaced due to depletion sources and their emission [2]. Environmentally friendly and sustainable source for electrical energy storage, such as supercapacitor, can be a solution to these issues. The supercapacitor has high power and energy density, rapid

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charging-discharging, long lifetimes, safety, and excellent en 28 performance [3].

There are two types of supercapacitors based on the ions storage mechanism [4]. First, there is the electrochemical double-layer capacitances (EDLC), where capacitance is the accumulation of ion pairs between electrolyte and surface electrode [5]. The second one is pseudo-capacitance, which has a higher capacitance 15 n EDLC. Its capacitance is the redox reaction generated from the interactions of the surface functionalities with the active species in the electrolyte [6]. However, the redox reaction could be considered corrosive for a current collector and higher resistivity of supercapacitor cells. Both above mentioned features lead to a decrease in power density, low conductivity, and poor cycle stability [7]. Therefore, EDLC is recommended for good cycle stability and electrical conductivity. It is an environmentally device without chemical reaction and electrolyte depletion [8].

To enhance the capacitance of EDLC, many researchers have focused on developing the properties of its electrode since capacitance is proportional to its specific surface area [9]. A large specific surface area promotes a larger active

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area in contact with the electrolyte for high energy storage [10]. Therefore, activated 52 bon with high porosity is suitable for EDLC electrodes due to the large surface area [8]. According to the storage mechanism of pure EDLC, activated carbon provides specific surface area and capacitance of 3000  $15 \text{ g}^{-2}$  and 300 F g<sup>-1</sup>, respectively [11, 12]. Additionally, pore volume and size distribution influence the performance of supercapacitor electrodes. The micropores (<2 nm) prom 38 jons storage to generate high energy performance. The mesopores (2–50 nm) and macropores (> 50 nm) reduce the pathway for ion diffusion, leading to 10 id mobility and reduced power loss [13]. In summary, large specific surface area and pore size combination are essential factors to be considered in designing activated carbon for supercapacitor electrodes.

Activated carbon with mique structures such as carbon nanofiber is advantageous in charge transfer and allows fast access of electrolyte ions to the surface of the electrodes [14]. Chen et al. (2008), obtained carbon nanofiber from biomass, including palm kernel shell, coconut, and wheat straw, through chemical vapor deposition (CVD) [15]. CVD directly produces carbon nanofiber without dissolving preparation with low fiber density. Moreover, the CVD process needs catalysts and conducted in high vacu 141 conditions [16]. The electrospinning method has been widely used to produce carbon nanofiber with high specific surface area and fiber density, excellent electrochemical performance, and lower energy process [17]. It is a commonly used polymer precursor, or carbon biomass mixing the polymer, which increases production cost [18]. Electrode production in the two-stage electrospinning process for converting a suspension into fiber and pyrolysis process takes a longer time [19]. Therefore, these methods are uneconomic and inefficient for ele 51 ode production.

To cut down the cost of production of the electrode, the biomass waste with nature fiber structure can be used as an alternative for supporting the facile method to produce carbon nanofiber [20]. It is abundant, easy to process, has zero cost, and can be performed in a wide range of temperatures, and providing pore and structure nature [21]. One stage integrated pyrolysis can promote an alternative for a facile method for producing activated carbon nanofiber [22]. Some biomass have been reported to become attractive precursors for activated carbon, including Rhus typhina fruits [23], palm oil [24], tea waste [25], pistachio shell [26], rice husk [27], mangosteen peels [28], banana peel [29], tree bark [30], lotus leave [31], cotton [32], egg white [33], strobili fibers [20], dandelion [34], dairy manure [35], and wild fungus [36]. Biomass contains a large amount of cellulose, hemicellulose, and lignin, which constitute tissue for pore and structure nature [37-39]. Celluloses can be extracted into nano-sized fiber due to the presence of elemental fibril [34, 40].

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Activated carbon from 18 mass was commonly studied as powder and monolith. Activated carbon powder has a higher specific surface area than a monolith, specifically 2700 mg<sup>-1</sup>, which increases electrochemical performance [23, 41]. However, it is not widely used due to dusting for further energy storage applications. The additive polymer for supercapacitor assembly leads to a loss of conductivity [42]. It is necessary to use monolith electrodes for good mechanical properties since it can be directly used for packaging. The monolith produces higher electrical conductivity, specific capacitance, and good cycling capability at high current densities [43].

Areca catechu fruit husk, a native of Southeast Asia, is an abundantly cultivated waste material. It is obtained in the range of 60–80% of its total weight and volume of the fresh fruit [44]. Its ripen nut has been used for industrial textile coloring, which produces abundant unutilized husk [45]. It contains cellulose (34.18%), hemicellulose (20.83%), lignin (31.60%), and a few minerals [44]. Based on structure, it is 40% fiber and has a diameter size ranging from 396 µm to 476 µm [46]. The fiber has a longitudinal arrangement and bonds the micr 53 pril structure [47]. Therefore, Areca catechu fruit husks can be used to produce activated carbon nanofibers for the monolith electrode.

This study reports a facile and low-cost method using one stage integrated pyrolysis to produce activated carbon nanofiber from the *Areca catechu* husk (ACH). The samples were prepared using chemical activation of KOH at different concentrations to show the morphology transformation from aggregat 8 nto a nanofiber. The activated carbon nanofiber of ACH has the highest spec 57 surface area of 838 m<sup>2</sup> g<sup>-1</sup> in the concentration of 0.7 M KOH. In a twoelectrode cell, the nanofiber structure compared to aggregate remarkab t3 ncreases the specific capacitance from 101.63 to 181.96 F g<sup>-1</sup> at a scan rate of 1 mV s<sup>-1</sup>, in the 1 M H<sub>2</sub>SO<sub>4</sub> electrolyte. These results show the great potential of *Areca catechu* fruit husk (ACH) for activated carbon nanofiber as a supercapacitor electrode.

#### 2 Experimental

#### 2.1 Materials and methods

The ripen *Areca catechu* husk (ACH) were collected from Riau province (Riau, Indonesia). The ACH sample was processed into the fiber for raw material preparation. Importantly, chemical materials such as Potassium hydroxide (KOH) and Sulfuric acid ( $H_2SO_4$ ) were based on Merck KGaA (Darm 8 dt, Germany). All chemical materials were chosen in the analytical grade and can be used without further purification.

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#### 2.2 Sample preparation

The ACH fibers were converted into powder via pre-carbonized and sieved of size of less than 53  $\mu$ m, following the previous study [48]. ACH 60 vder was treated with KOH at different concentration (0 M, 0.3 M, 0.5 M, 0.7 M, 0.9 M). The samples were labeled ACH-X, where X was the concentration of KOH. All ACH-X were molded into a pellet of diameter  $\pm 2$  cm, which was pressed by a hydraulic press. Subsequently, 3 ACH-X pellets were converted into activated carbon via one-stage integrated pyrolysis both of carbonization (600 °C N<sub>2</sub>) and physical activation (900 °C CO<sub>2</sub> for 2.5 h), following the previously study [48]. Finally, the activated carbon from ACH-X pellets was purified using deionized water until neutral PH and polished for electrode supercapacitor preparation.

#### 2.3 Structure characterization

The mass, diameter, and thickness were measured to determine the density of ACH-X pellets before and after the pyrolysis process. The morphol 26 structure of activated carbon from ACH-X pellets was characterized by scanning electron microscopy (SEM) (JEOL-JSM-6510LA) and embedded wit 14 ergy dispersive x-ray spectroscopy (EDS). Additionally, specific surface area (SSA) was determined using the Brunauer Emmett Teller (BET) adsorption model (Quantachrome TouchWin Version 2). The pore size distribution was based on the desorption branch of the isotherms, calculated using the Barrett–Joyner–Halenda (BJH) method. The crystallinity degree of the ACH-X samples was investigated using an X-ray diffractometer (XRD) (X-Pert Powder PW 30/40 and a wavelength of Cu-Kα 15,406 Å).

#### 2.4 Electrochemical performance evaluation

The pellet based activated carbon of ACH-X was immersed in a liquid electrolyte of 1 M  $H_2SO_4$  for 48 h. Subsequently, the ACH-X pellets were utilized as electrode supercapacitors. They were assembled in the symmetrical layers, which was separated by separator using an duck egg shell. The preparation of separator was explained in detail in the previous work [49]. stainless steel was used as a current collector with the voltage range of 0.0–1.0 V. The symmetric supercapacitor was performed on **3** e CV UR Rad-Er 5841 instrument. It was calibrated to VersaStat II Princeton Applied Research, with an error of  $\pm 6.05\%$ . The CV measurement was conducted in two electrodes systems **2** pproaching the real utilization of energy storage devices. To investigate the electrochemical performance, the specific capacitance was calculated following the Eq. (1) below.

$$C_{sp} = \frac{I_c - I_d}{m \times s}.$$

(1)

The energy and power densities were calculated from CV using the Eq. (2) and (3), respectively.

$$E = \frac{1}{2}C_{\rm sp}\Delta V^2 \times \frac{1000}{3600},\tag{2}$$

$$P = \frac{E}{\Delta t/3600},\tag{3}$$

where  $C_{sp}$  is the sp2 ific capacitance (F g<sup>-1</sup>), while  $I_c$  and  $I_d$ are the charge and discharge current (A), respectively. Als 2 *m* is the average mass loading of two electrodes (g) while *E* is the average energy density of the electrod (Wh kg<sup>-1</sup>).  $\Delta V$ and  $\Delta t$  are the potential window of CV (V) and discharge time in the discharge process (*s*), respectively. *P* is the average power density of the electrode (W kg<sup>-1</sup>).

#### 3 Result and discussion

#### 3.1 Density

At high temperature, pyrolysis changes the pellet of the monolith activated carbon from ACH-X. The diameter, thickness, and mass of ACH-X pellets were resumed in the density variable, as shown in Fig. 1. The data was calculated from 10 pellets for each sample, and the results showed pyrolysis reduced density. The carbonization process at the high temperature of 600 °C releases some of the low molecular weight volatiles, such as oxygen, nitrogen, and hydrogen, reducing the mass of the pellets [13]. Besides, the physical activation



Fig. 1 Density diagram of the activated carbon from ACH-X

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of  $CO_2$  produced residues such as carbon monoxide in the gaseous phase [43]. The volatiles released to generate the vacancies in the carbon chains leading to rearrangements that reduced both the pellet diameter and thickness.

The chemical activating agent of KOH increases the density of the pre-carbonized ACH-X samples before pyrolysis from 1.079 to 1.21 g cm-3 for ACH-0 and ACH-3, respectively. This due to impregnate of the higher molecular weight of KOH into carbon biomass. As the concentration of KOH increases, the density remains the same for ACH-3, ACH-5, ACH-7, and ACH-9, specifically 1.21, 1.21, 1.21, 1.20 g cm-3. The pellets preparation was conducted at a constant mass, size of the template, and the weight of hydraulic press. It was assumed that there was no significant effect on pellet density before pyrolysis, though the chemical activation influenced the density after the process. Essentially, it shrank at the different ratios, including 22.5%, 14.9%, 30.1%, 33.2%, and 46.2% for ACH-0, ACH-3, ACH-5, ACH-7, and ACH-9, respectively. The increase in the concentration of KOH raised the new micropores formation [13, 50]. This led to high porosity and specific surface area, which improved electrochemical performance. Therefore, increasing concentration from ACH-7 to ACH-9 decreases the density significantly. It indicates the higher porosity and enlarges the micropores to larger pores [50, 51]. These results indicate that electrochemical performance for ACH-9 reduces as predicted.

#### 3.2 Structural characteristic

As shown in Fig. 2, the morphology of carbon samples was observed by scanning electron flcroscopy (SEM). The morphology and structure of the activated carbon derived biomass materials was affected by raw materials, activating agent and the treatment to convert it into carbon material [13]. Generally, biomass materials contain cellulose,

Fig. 2 SEM images of samples (a) ACH-0 (b) is the enlarged image of the selected region in (a) (c) ACH-3 (d) is the enlarged image of the selected region in (c) (e) ACH-7 (f) is the enlarged image of the selected region in (e)



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hemicellulose, and lignin [37, 38], which have the potential to develop into any structures of carbon materials, including carbon sheet [52], fiber [20], nanotubes [32, 48], and particles [53]. Additionally, they provide natural pores, though the disordered carbon atoms and heteroatoms block them [21, 42]. The KOH activating agent was impregnated into pre-carbonized ACH for fabricating nanofiber and porous carbon. The activation process of KOH was carried out in one stage integrated pyrolysis with both carbonization and physical activation. During the carbonization, the low molecular weight of volatiles such as oxygen, nitrogen and hydrogen changed into the tars and gases [13]. Hence, they were released in the gas phase, leading to carbon atom rearrangement. In addition, the physical activation in the high temperature facilitated pore development through gasification reaction between ACH char and CO<sub>2</sub> [43].

Figure 2 show the SEM image of activated carbon electrode from ACH-x samples. The pelletizing process on synthesis of carbon electrode generated some open pores network between adjacent aggregate of ACH. Figure 2a shows that activated carbon derived from ACH-0 without KOHimpregnated have an aggregate-like structure in size ranging from 3.02 to 4.03 µm. There are some open pores network between the aggregates, though within 0.51-0.97 µm. It is also clear that ACH-0 have various range of aggregates as shown by the marked region in the Fig. 2b. The aggregate size and open pores network ranged from 0.28 to 0.47 µm and 35-84 nm, respectively. Hence, the supramolecular of ACH-0 raw materials decomposed into aggregate structures due to pyrolysis [14]. In the first step, the carbonization process at the temperatures of 600 °C under N2 decomposes the hemicellulose and cellulose structure [21, 54]. In the second step, the lignin structure in the ACH-0 decomposed due to the physical activation at the temperature 900  $^{\circ}C$  [14, 38]. Additionally, physical activation achieved the reaction at between a carbon atom of ACH and CO<sub>2</sub> at the surface. This produced the gaseous residue of carbon monoxide, opening inaccessible pores [43]. This further predicts the open pores network of ACH-0 which produce specific surface area and supports ion diffusion into mesopores and micropores.

Meanwhile, KOH activation leads to structural modification on the ACH-3 from large to small aggregate and nanofiber decorated, as shown in Fig. 2c. The aggregate carbon obtained ranged between 1.79 and 3.79  $\mu$ m in size. The figure also depicts a smooth surface and some open pores network in the aggregate carbon ranging from 0.52 to 1.21  $\mu$ m in size. Moreover, there are multilayer nanofibers onto the aggregate carbon surface and twig fiber structure, as shown by the marked region in Fig. 2d. The nanofiber had a diameter ranging from 65 to 119 nm. Initially, the carbon structure was modified by chemical activation. During the KOH-impregnated process, hemicellulose was extracted by alkaline, leaving numerous lignin and cellulose [55]. This leads to the conversion of a sizeable aggregate structure into a small aggregate and nanofiber of ACH-3. Meanwhile, the chemical activation process also supports micropores formation [13, 38, 43]. KOH reacted with carbon atom during the carbonization process under the protection of inert gas. It produced main products, forming carbon, potassium, and potassium carbonate [43]. Additionally, some gases, including hydrogen, carbon dioxide, carbon monoxide, and water vapor were also produced and released at high temperatures [13, 38]. In the next stage, physical activation continu 7 sly enlarged the micropores and completely collapsed the walls between adjacent micropores to form larger pores [13, 43].

Furthermore, a higher concentration of KOH in the ACH-7 increased the number of the fiber and generated new pores onto the rough aggregate surface, as shown in Fig. 2e. Aggregate carbon and the open pores network were reduced in the range of  $0.81-2.98 \ \mu\text{m}$  and  $0.18-1.52 \ \mu\text{m}$ , respectively. There was a single structure nanofiber without twig and multilayers, as shown by the marked region in Fig. 2f. The nanofiber diameter was also reduce 49 in the range of 51-89 nm. It also depicts that the new pores on the surface of aggregate carbon were formed. Initially, the increasing concentration of KOH produced more residual product which was K2CO3-occupied and K-bound at the high temperature [43]. This condition leaves numerous vacancies on the monolithic electrodes of ACH-7, either aggregate or nanofiber. It leads to generate more micropores onto the surface of aggregate carbon [13, 50, 51]. The physical activation at the high temperature of 900 °C enlarged the existed micropores into mesopores or macropores [13, 43]. Moreover, a higher concentration of KOH removed more hemicellulose and increased the degradations of lignin at the high temperature [55]. It rearranges the remaining carbon atom, increasing the number of the nanofiber but at the same time reducing their diameter. Finally, the residual product of activation was removed from the activated carbon by washing. Further, it predict 56 e aggregate fiber decorated in ACH-3 and ACH-7 had high specific surface area and electrochemical performance. 39

The N<sub>2</sub> adsorption/desorption isotherms were used to further analyze the specific 48 ace area and pore structures in the carbon samples 27 shown in Fig. 3a. All the samples exhibit the typical IV isotherm according to the international uni 3 of pure and applied chemists (IUPAC). The isotherm's significant increase in volume at the low relative pressure (P/P<sub>0</sub> < 0.36 indicates the presence of micropores [25, 39, 50]. The hysteresis loop at high relative pressure (P/P<sub>0</sub>=0.4–0.95) indicates the presence of numerous mes 3 ores [29, 31, 51]. Therefore, all the samples of ACH-X exhibit well-developed combination of micropores and mesopores. The isotherm of ACH-0 and ACH-7 shows normal hysteresis, which the adsorption/desorption is almost equal. It correlates with the SEM image (see Fig. 2a–b for

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Fig. 3 Textural characteristic of ACH-X samples (a) Nitrogen adsorption-desorption isotherms (b) and pore size distribution

Table 1 The textural properties of ACH-X carbon samples

Samples	Specific surface area $(m^2 g^{-1})$		Pore volut ( $cm^3 g^{-1}$ )	D <sub>average</sub> (nm)	
	S <sub>BET</sub>	S <sub>BJH</sub>	V <sub>TOTAL</sub>	$V_{BJH}$	
ACH-0	696.689	35.300	0.375	0.040	2.136
ACH-3	754.974	41.712	0.403	0.050	2.151
ACH-7	838.636	23.642	0.448	0.032	2.137

ACH-0 and d–f for ACH-7), either macropores for ACH-0 or single layer nanofiber for ACH-7. Therefore, it reduces pore-blocking during the desorption process at low relative pressure. Furthermore, the isotherm of ACH-3 has unique hysteresis loop that displays a higher desorption volume than adsorption. This condition indicates the presence of unique textural in the ACH-3 samples. In reference to SEM image (see Fig. 2b–c), the ACH-3 displays the multilayer structure of nanofiber, blocking the desorption flow at low relative pressure [56]. Furthermore, the presence of a nanofiber structure suggests high specific surface area of ACH-X carbon samples.

The surface-specific area and pore structure parameter of all carbon samples are summarized in the Table 1. With increasing concentration of KOH in th 10 lectrodes from ACH-0, ACH-3, and ACH-7, the specific surface area ( $S_{BET}$ ) increases from 696, 754, to 838 m<sup>2</sup> g<sup>-1</sup> with the total pore volume ( $V_{TOTAL}$ ) of 0.375, 0.403, and 0.448 cm<sup>3</sup> g<sup>-1</sup>, respectively. Additionally, the ACH-0, ACH-3, and ACH-7 have an average pore diameter of 2.136, 2.151, and 2.137 nm, respectively. As the alkali ratio in the carbon samples incr 47 s, the micropores formation also increases [50, 51]. As shown in Fig. 3b, the pore size distribution of ACH carbon samples were investigated by Barrett Joiner Halenda (BJH) model. The dominant pore sizes were 3.596, 3.528, 3.556 nm for ACH-0, ACH-3, and ACH-7, respectively. It was found that



Fig. 4 XRD diffractogram of ACH-X samples

the pores size measured by BJH method were in the range of mesopore sizes (2–50 nm). Moreover, the surface area and tot  $\frac{5}{2}$  mesopore volume was obtained of 35.300, 41.712, 23.642 m<sup>2</sup> g<sup>-1</sup> and 0.040, 0.050, 0.032 cm<sup>3</sup> g<sup>-1</sup> for ACH-0, ACH-3, and ACH-7, respectively. In ACH-3 samples, using KOH as an activating agent followed by physical activation at high temperature enlarged micropores and increased mesopore [50]. The other hand, as increasing concentration of KOH in the ACH-7, it enlarged the existed micropores to macropores by collapsing the walls between their adjacent micropores [13]. The presence of macropores in carbon samples increases the ion diffusion rate to mesopore and micropores [23, 57]. It predicts the best performance for electrocl 46 ical performance.

XRD measurements were performed to confirm the crystalline structure of all samples. As shown in Fig. 4, the samples have two broad peaks at around  $2\theta$  angles, precisely  $24^{\circ}$ 

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and 44° for the carbon planes 002 and 100, respectively. The carbon planes of all samples ACH-X are the typical agreement with the amorphous structure of carbon materials [38], similar with carbon biomass from peanut shell [58], albizzia flower [41], peach gum [59]. The pyrolysis or carbonization process of carbon derived biomass materials obtained amorphous structure [60]. Furthermore, the amorphol 45 arbon provides the porous carbon with the high porosity and large specific surface area [38]. The impure carbon of biomass materials shows the sharp peaks of the ACH-3 diffractogram. It has a high molecular weight that does not release high temperature for the activation process. In the ACH-3 samples, the presence of the impurity at around  $2\theta$  angles 28° indicated a small amount of silica  $ox_{3c}$  (SiO<sub>2</sub>) [24].

The lattice parameters, which include interlayer spacing  $(d_{002} \text{ and } d_{100})$  and microcrystalline (L<sub>c</sub> for stack height and L<sub>a</sub> for the stack width) structure were resumed in Table 2. The interlayer spacing was calculated using Br 24 's Law  $(n\lambda = 2d \sin 2\theta)$ , where n is diffraction order (n = 1),  $\lambda$  is the wavelength for the X-ray beam ( $\lambda = 1.5406$  Å), and 2 $\theta$  is the angles of XRD diffraction. The carbon planes from ACH-X samples have a good agreement with carbon materials at the interlaying spacing around 3.6 Å and 2.0 Å for 002 and 100, respectively. For example, activated carbon from empty fruit bunch of palm oil demonstrated a d<sub>002</sub> between 3.692 and 3.711 Å [24]. The microcrystalline din 22 sion was evaluated from Debye–Scherrer formula  $(L_c = 0.89\lambda/\beta cos(\theta_{002}))$  and  $L_a = 1.94 \lambda / \beta \cos(\theta_{100})$ , where  $\beta$  is equal to the peak width at half height [24, 61]. As shown in Table 2, the KOH activating agent have reduced  $L_c$  and increased  $L_a$ . The KOH activation in the high temperature supports to release the im 35 rity and rearrangement of the carbon atom. The higher  $L_a$  for activated carbon may be caused by either sp<sup>3</sup> or interlayer repulsion, due to negatively charged of functional surface [61]. Furthermore, the ratio of  $L_c/L_a$  predicts the high porosity of ACH-X samples at a low ratio [24]. The  $L_c$  number affected the specific surface area in inverse correlation in Kumar empirical formula  $(S=2/(\rho L_c))$ , where S is the predicted surface area, and  $\rho$  is the density of the graphite [62].

The EDS analysis reveals the chemical composition of ACH-X sample 1 which were resumed in Table 3. The integrated stage in both carbonization and physical activation successfully converts biomass into activated carbon of ACH materials. Activated carbon of ACH-X contains the carbon with an atomic weight of 85.12% for ACH-0. Generally, with

Table 3	Chemical	composition	analysis c	of ACH-X	measured	by EI	)S
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Chemical contents	Atomic weight (%)					
	ACH-0	ACH-3	ACH-7			
Carbon	85.12	90.59	89.34			
Oxygen	11.11	7.68	8.46			
Magnesium	0.35	0.20	0.23			
Silica	2.28	1.07	1.17			
Potassium	0.56	0.31	0.80			
Chloride	-	0.15	_			
Zinc	0.28	-	-			
Sulfur	0.30	-	_			
Total	100	100	100			

chemical activation of KOH, the carbon content increased while oxygen decreased. The chemical activation of KOH etches the carbon-compounds bond, leading increase the carbon contained [43]. Meanwhile, low molecular weight and bad thermal stability at the high temperature limits the amount of oxygen released [29]. The increase in the concentration of KOH slightly decreased the carbon contents from 90.59% to 89.34% for ACH-3 and ACH-7, respectively. This is attributed to the increase in the oxygen contents from 7.68 to 8.46% for ACH-3 and ACH-7, respectively, which is the product of chemical and physical activation [5, 37]. However, the oxygen might contribute to be chemically absorbed in H2O and/or C-OH, improving the hydrophilicity of electrode materials. For aqueous electrolyte, the hydrophilicity associated to ion adsorption from liquid electrolytes to the active specific surface area of electrode [25, 63]. It provides the best electrochemical performance for ACH-7, as predicted.

The Si is the common residual product that was obtained by the pyrolysis process for activated carbon fabrication derived biomass materials [29, 48, 64]. The other elements contained include magnesium and zinc, depending on the composition of cultivated soil [60]. A few amounts of the elements may remain after chemical and physical activation due to high molecular weight. The chloride can be obtained as the natural content of raw ACH-X, that could be released as gaseous phase at high temperature [38], depending on nominal composition. The other mineral in ACH-X activated carbon is sulfur, which can be removed by washing after chemical activation [60]. Potassium is the natural content of

Table 2         XRD parameters of all           ACH-X samples	Samples	2θ <sub>002</sub> (°)	2θ <sub>100</sub> (°)	d <sub>002</sub> (Å)	(Å)	L <sub>ç</sub> (Å)	L <sub>a</sub> (A)	L <sub>c</sub> /L <sub>a</sub> (Å)
	ACH-0	24.760	44.084	3.592	2.052	11.916	30.517	0.390
	ACH-3	24.035	44.066	3.699	2.053	10.754	46.337	0.232
	ACH-7	24.658	43.910	3.607	2.060	9.707	69.788	0.139

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biomass [38], although it increases in the chemical activation of KOH due to imperfectly washing [48].

#### 3.3 Electrochemical characteristic

ACH-X samples were prepared for working electrodes to investigate the capacitive performance using cyclic vol 4 mmetry (CV). ACH-X samples were assembled in the tw 23 electrode system, and the CV tests were carried out in 1 M  $H_2SO_4$  electrolyte at the scan rate of 1 mV/s, as shown in Fig. 5a. The CV curves depict the rectangular-liked shape, which suggests the ideal double-layer capacitance of samples [31, 35]. In general, the CV curve area represents the charge–discharge rate, which determines the capacitance value.

The CV curve area of ACH-7 is largest for all ACH samples, which indicates that ACH-7 exhibits best electrochemical performance as predicted. In general, the specific capacitances (*Cs*) calculated from Eqs. (1) increase from 101.63, 117.31, and 120.24 to 181.96 F g<sup>-1</sup> for ACH-0, ACH-3,

ACH-5, and ACH-7, respectively, and drops for ACH-9 of 169.26 F g<sup>-1</sup>. Notably, the increasing concentration of KOH in the ACH-X samples increased capacitance. For ideal specific capacitance, either the pores properties or carbon structure played critical roles in the storage and transport of electrolyte ions [71]. As discuss previously, the increasing concentration of KOH is attributed to expose the high SSA and the large number of pores volume. This condition provides sufficient active sites for ion pairs from both electrolyte ion and accessible surface area of activated carbon [31]. As the concentration of KOH increases in the ACH-9 samples, the pores structure may collapse and the SSA decreased. Table 4 shows the performance comparison of ACH with the biomass carbon based-nanofiber structure reported 13 ted, in the two-electrode system. It performs that ACH exhibits a high specific capacitance of 181.96 F g<sup>-1</sup>.

As slown in Fig. 5b, ACH-7 depicts steady rectangular-like shapes of CV curves at different scan rates from 1 to 2 mV/s. This condition indicates that the ACH-7 has fast ion transport ability. As discuss previously, the open



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 Table 4
 Various precursors

 based-activated carbon as
 supercapacitor electrodes in

 two-electrodes system
 two-electrodes system

Precursors	Nanofibers	Activator agent	$\begin{array}{c} S_{BET} \\ (m^2 \ g^{-1}) \end{array}$	Cs (F g <sup>-1</sup> )	Electrolyte	Refs
Tea leaves	_	КОН	911	167	12 Na <sub>2</sub> SO <sub>4</sub>	[25]
Albizzia flower	-	КОН	2757	58	1 M Na <sub>2</sub> SO <sub>4</sub>	[41]
Mangosteen peels	-	KOH	1270	83	6 M KOH	[28]
Banana peels	-	КОН	1362	165	1 M NaNO <sub>3</sub>	[65]
Dairy manure	-	КОН	1651	202	6 M KOH	[35]
Soybean	-	KOH	1749	116	$0.5 \text{ M} \text{Na}_2 \text{SO}_4$	[51]
Lumpy bracket	-	КОН	1968	223	6 M KOH	[61]
Waste tea	-	ZnCl <sub>2</sub>	923	140	6 M KOH	[63]
Setaria viridis	-	КОН	701	199	6 M KOH	[66]
Glebionis coronaria	-	_	1007	205	6 M KOH	[67]
Starch	-	КОН	2259	81	2 M KOH	[68]
Orange peel	-	КОН	1577	168	6 M KOH	[69]
Corn leaf	-	$H_3PO_4$	2507	230	$1 \text{ M} \text{H}_2 \text{SO}_4$	[70]
Areca catechu husk	Nanofiber	КОН	839	182	1 M H <sub>2</sub> SO <sub>4</sub>	[This study]

pores network structure of ACH-7 can provide ion transport channels at high charge/discharge rates [23]. Furthermore, the micropores and mesopores of ACH-7 supplies a large amount of the accessible surface area for ion buffering and storage [25, 31]. In addition, the nanofiber structure of ACH-7 provide high SSA which ensure simply accessible interface for fast diffusion of electrolyte ions [14].

Calculated from CV curves at different scan rate 19 e specific capacitance of ACH-X samples were resumed as shown in Fig. 5c. 43c specific capacitance (Cs) of ACH-X samples decreases with the increase in the scan rate. The specific 55 acitance of ACH-0, ACH-3, ACH-5, ACH-7, and ACH-9 at the scan rate 2 mV/s slight34 drops to 93.12, 80.09, 94.24, 89.00 and 76.53% of that at a scan rate of 1 mV/s, respectively. Acc21 ing to these results, the Cs value slightly decreases as the scan rate increase from 1 to 2 mV/s, implying that the ACH-X samples have a rapid ion transport to active SSA [23]. Furthermore, the unique trend of the Cs shows at the scan rate 5 to 10 mV/s, which significantly decreases for ACH-3, ACH-5, and ACH-7. From the previous discussion of morphology (see Fig. 2a-f), chemical activation using KOH increases the number of micropores formed. This is confirmed by the increase in the specific surface area and mesopore decrease (see Table 1). These conditions lead to an increase in the resistivity for ion diffusion, resulting low the Cs at high scan rate [25]. Meanwhile, the Cs of ACH-0 and ACH-9 is much higher than ACH-7. These results associated to better accessible SSA, provided by the larger open pores network between adjacent the aggregate for ACH-0, and the collapsing walls of the 3 res on the high KOH concentration for ACH-9. In addition, at the highest scan rate of 10 mV/18 it remains to be 37.27, 23.54, 24.31, 15.96, and 24.71%. It can be concluded that both the pores and unique structure of activated carbon electrode affects ion diffusion to the active SSA, which determines the ion buffering and storage [71].

The ACH-X samples obtained the high energy densities of 14.11, 16.29, 16.70, 25.27, 23.50 Wh kg<sup>-1</sup> for ACH-0, ACH-3, ACH-5, ACH-7, and ACH-9, respectively. While the power densities also were achieved of 50.86, 58.71, 60.18, 91, 07, 84.71 W kg<sup>-1</sup> for each sample of ACH-0, ACH-3, ACH-5, ACH-7, and ACH-9. These results regard the energy and power density for activated carbon biomass electrodes. For example, activated carbon from lotu 29 aves exhibits the energy density between 25.76 and 30.28 Wh kg<sup>-1</sup> and power density of 180 W 25<sup>-1</sup> [31]. Activated carbon from soybean demonstrated the energy density of 12.5 Wh kg<sup>-1</sup> and power density of 450 W kg<sup>-1</sup> [51].

Therefore, it was found that the specific capacitance (Cs) value was affected by physical properties and chemical element, such as; (1) low density of pellet carbon electrode might provide high porosity for ion capturing; (2) a unique structure of nanofibers serves b42 r surface accessibility and large specific surface area; (3) high specific surface area and large pore volume provides much ion pairs formation; (4) highly carbon composition indicates to high electrical conductivity of carbon electrode; (5) also, more oxygen content might contribute to increase the hydrophilicity degree for better ion adsorption in aqueous electrolyte; (6) highly disordered carbon atom by amorphous structure might generate the large surface of electrode, resulting high specific capacitance (Cs).

#### 4 Conclusion

In summary, carbon nanofiber in monolith form were prepared from sustainable and green precursor *Areca catechu* husk (ACH) based cellulose microfibril through chemical

activation at different concentrations of KOH. Chemically activation of ACH samples transformed aggregate into nanofiber structure, by just one conventional route of integrated stage pyrolysis both carbonization and physical activation. The furth 10 chemical activation developed nanofiber structure, led to a large specific surface area and high pore volume, which is beneficial for achieving high electrochemical performance 5 Also, the optimized ACH-7 samples show a large specific surface area of 838.64 m<sup>2</sup> g<sup>-1</sup> with a total pore volume of 0.448 cm<sup>3</sup> g<sup>-1</sup>. Sym 41 ric supercapacitor fabricated form ACH-7 exhibits the 20 hest specific capacitance of 181.96 F g<sup>-1</sup> and maximum energy density of 25.27 Wh kg<sup>-1</sup> for the power density of 91.07 W kg<sup>-1</sup> in 1 M H<sub>2</sub>SO<sub>4</sub> electrolyte. This study show 7 greement the presence of nanofiber structure increases charge transfer and provides fast access for electrolyte ion into the surface of electrodes. This work provides a facile one conventional route of integrated pyrolysis to convert biomass Areca catechu husk into carbon nanofiber for high-performance electrode supercapacitor.

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